Progress on a Passive System for Turbidity Control in Construction Site Runoff

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## **Project Team**

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# **Overall Objectives**

- Develop a predictive flocculation model for design and permitting purposes
- Design and test a passive liquid flocculant dosing apparatus suitable for construction site implementation

# Outline

- Background
- Methods and Preliminary Results
  - Passive injection/mixing system concept and modeling
    - Flocculent selection/jar tests
  - Concept for measuring flocculation constants
- Continuing work including expected finish date

### **Sediment Management Strategies**

- Erosion Control
  - Surface Armoring
  - Hydraulic Energy
    Dissipation

radodot.info/programs/en

ronmental/water-quality/assets/checkdam-rock-good.jpg

- Sediment Capture
  - Sediment detention ponds



http://www.colemanmoorecompany.com/article.asp?

articleid=5926





http://www.burchlandmfg.com/erosio n\_control\_products.php



### Enhanced Sedimentation Using Chemical Flocculants

- Proven technology utilized in wastewater treatment
- Potential to significantly increase onsite sediment capture
- Reduce runoff turbidity
- Decrease required sediment retention pond volume

### How does flocculation work?

Flocculation refers to the bridging between particles by a polymer chain, causing them to form flocs or larger aggregates. These flocs float (flotation) or sink (sedimentation), making them easier to remove from the system.



From: tramfloc.com

### **Equations for Flocculation**

- Based on the binary model for flocculation based on the work done by Argaman and Kauffman (1971)
- Mathematical equations for determining the rate of floc formation and floc break up are

$$\frac{dn_p}{dt} = -(H_{1F}) + (B_{RF})$$

**Floc Formation:** 

$$H_{1F} = \alpha 4\pi K_S R_F^3 n_1 n_F \overline{u'^2}$$

Floc Break-up:  
$$B_{RF} = B R_F \frac{n_F}{R_1^2}$$

α = Fraction of collision resulting in successful flocculation

 $K_s = Flocculation constant (sec/ft<sup>2</sup>)$ 

- B = Floc break up constant
- $n_1$  = Number of primary particles
- n<sub>F</sub>= Number of flocs
- R<sub>1</sub>= Radius of primary particles
- $R_f$  = Radius of the flocs
- u<sup>2</sup> = Root mean square velocity

### Current Onsite Flocculation Technologies

Soldier Field Chicago, IL Winter/Spring 2002. Companies Inc.. Wyoming, MI and Wixor





http://wecleanwater.com/html/equipment dewatering/slurry\_system.htm

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### Methods and Some Preliminary Results

### **Passive Liquid Injection Devices**

#### **Floating bucket**

- Rainfall controlled dosing
- Proven feasible
- Simple operating concept
  and construction
- No moving parts



#### **Experimental Design**

- Runoff controlled dosing
- Simple design and calibration
- Simple installation

What range of dosing concentration can be achieved by each system?

# **Conceptual Layout of Experimental Design**



### **Passive System Modeling**

#### **Floating bucket**

- Changing onsite characteristics impact operation
- Must rely on synthetic storm to design system
- Must be designed on a site to site basis

#### **Experimental System**

- Doses based on runoff so system is independent of site conditions
- Generalized designs are possible based on expected runoff volumes

### **Floating Bucket System Modeling**



### **Floating Bucket System Modeling**



Square (1:1 l:w) Construction Site

#### Minimum Maximum

Acres	(min)	(min)
1	3	3
2	4	5
3	4	6
5	5	8
10	7	11

### **Experimental System Modeling**



### **Jar Tests**

- The behavior of each soil/flocculant combination is different
- To start with, we are completing jar tests to determine:
  - Type of flocculant to use
  - Velocity gradient to use
  - Concentration of flocculant to use

### **Jar Test Methods**

- 66 second pre-settling (from Stokes equation)
- 5 second mixing
- 4 minute post-settling
- Turbidity measured and TSS analyzed

### **Jar Test Results**

Floc	Pros	Cons
	Greatest removal efficiency	
	Long stability in concentrated	
Hydrofloc	form	Very high viscosity
	High removal efficiency	Difficult to mix
Superfloc 705	Moderate viscosity	Very short stability
	Easy to mix	
FloPam SH	Low viscosity	Short stability
(solution)	High removal efficiency	Difficult to mix
FloPam VLM	High removal efficiency	
(solution)	Moderate Viscosity	Very short stability

### **Flocculation Modeling**

- Argaman and Kauffman (1971) showed that growth maximum size to which the flocs can grow is controlled the velocity gradient 'G' (sec<sup>-1</sup>)
- G is the function of the turbulence that can be generated in the sedimentation basin.
- The estimation of G values will be achieved by a set of oscillating grids in a flume with sediment flow at constant rate.
- The kinetic energy imparted by the grids will be used to estimate the G value which is given by

$$G=\sqrt{\frac{\varepsilon}{\vartheta}}$$

where; ε = Kinetic energy dissipated by the oscillating grids in one cycle

 $\vartheta$  = Kinematic viscosity of the fluid

### **Flocculation Modeling**

Schematic diagram for the oscillating grids:



### **Preliminary Conclusions**

- Design for passive injection and mixing system selected
- For our preliminary design, we will be using diluted Hydrofloc as our flocculent
- Design for flocculation parameter estimation apparatus selected and under construction

### **Continuing work...**

- Field testing of injection and mixing apparatus
- Continue jar tests on diluted Hydrofloc to estimate flocculent concentrations and velocity gradients necessary for optimum flocculation
- Testing of two soils to detemine flocculation parameters
- End date: June 30, 2011

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# **Questions???**